

[3 Hours]

[Total Marks: 80]

Instructions to the candidates if any: -

1. Question No 1 is compulsory
 2. Attempt any three questions from the remaining five questions
 3. Assume suitable data wherever necessary
 4. The figures to the right indicate full marks
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Q. No. 1

- a. As a chemical engineer how will select the solvent to be used in gas absorption? [05]
- b. Discuss the diffusion process of various solute through polymers. [05]
- c. Discuss the concept of wet-bulb temperature. [05]
- d. A thin film of liquid is flowing past a vertical surface, inclined at an angle of 30° with the vertical. The density of the liquid is 998 kg/m^3 , viscosity is $8.94 \times 10^{-2} \text{ kg/ms}$. The thickness of the liquid film is 2 mm . Find the bulk average velocity with which the film is coming down. [05]

Q. No. 2

- a. What do you mean by the unicomponent diffusion of liquid A in its binary mixture with liquid B? Derive an equation for the steady state mass transfer flux in this case. [08]
- b. The solute HCl is diffusing through a thin film of water 2.5 mm thick at 293 K . The concentration of HCl at point 1 at one boundary of the film is 13 wt \% HCl (Density of 1060.7 kg/m^3), and at the other boundary at point 2 it is 7 wt \% HCl (Density of 1030.3 kg/m^3). The diffusion coefficient of HCl in water is $2.5 \times 10^{-9} \text{ m}^2/\text{s}$. Assume steady state and one boundary impermeable to water, calculate the flux of HCl in $\text{kmole/m}^2\text{s}$. [12]

Q. No. 3

- a. A gas phase is in contact with a liquid and solute A is transferring from the gas phase to the liquid phase. Draw the concentration profile for this interphase phase transfer. Also, derive the relationship between individual and overall mass transfer coefficients. [10]
- b. Water is flow down a vertical wall 2.5 m long in the form of a thin film. The flow rate for the falling film is 0.045 kg/s per meter width at 25°C and 1 std atm . The water film is in contact with pure carbon dioxide. The solubility of carbon dioxide in water at 25°C is 0.0336 kmole/m^3 of solution and water is essentially free of carbon dioxide initially. The diffusion coefficient of carbon dioxide in water at the prevailing conditions is $1.96 \times 10^{-9} \text{ m}^2/\text{s}$. The density of the solution is 998 kg/m^3 and its viscosity is $8.94 \times 10^{-4} \text{ kg/m.s}$. Estimate the rate of absorption of carbon dioxide in water. [10]

Q. No. 4

- a. Compare tray columns with packed columns considering the following points. [08]
- | | |
|----------------------------|------------------------------|
| 1. Gas-side pressure drop. | 5. Presence of solids |
| 2. Liquid hold-up | 6. Temperature fluctuations. |
| 3. Liquid to gas ratio | 7. Cleaning |
| 4. Foaming systems | 8. Corrosion |
- b. A plant manufacturing dry ice will burn coke in air to produce a flue gas containing 15 % CO_2 , 6 % O_2 and 79 % N_2 . The gas is blown into a counter current absorption tower at 1.2 *std atm* and 25°C, to be scrubbed with 30 % ethanolamine solution containing 0.058 mole fraction of CO_2 in it. The gas leaving the absorption tower is to contain 2 % of CO_2 by volume.
- Determine the minimum liquid to gas ratio.
 - Determine *kg of entering liquid/m³ of the entering gas*, for liquid to gas ratio which is 20 % more than the minimum ratio.

The equilibrium data is given in the following table. $x_{CO_2}^*$ is the mole fraction of CO_2 in the liquid solution and $P_{CO_2}^*$ is the partial pressure of CO_2 in the gas mixture in *mm of Hg*

$x_{CO_2}^*$	0.058	0.060	0.062	0.064	0.066	0.068	0.070
$P_{CO_2}^*$	5.6	12.8	29.0	56.0	98.7	155	232

[12]

Q. No. 5

- a. Derive the equation for adiabatic saturation curves [08]
- b. 220 *kg* of a wet solid is to be dried from an initial moisture content of 26 % to a final moisture content of 3.5 %. Drying tests show that the rate of drying is constant at $3 \times 10^{-4} \text{ kg/m}^2\text{s}$ in the region $0.2 - 0.4 \frac{\text{kg water}}{\text{kg solid}}$. The drying rate falls linearly in the range of $0.01 - 0.2 \frac{\text{kg water}}{\text{kg solid}}$. If the equilibrium moisture content is $0.01 \frac{\text{kg water}}{\text{kg solid}}$, calculate the time of drying. The drying surface is $\frac{1 \text{ m}^2}{48 \text{ kg dry solid}}$ [12]

Q. No. 6

Write short notes on the following (Any four)- (20)

- Packings used in packed columns
- Minimum liquid to gas ratio in gas-absorption
- Venturi Scrubber
- The typical rate of drying curve
- Operational problems with tray columns
