## N. B.: (1) Question No. 1 is Compulsory.

(2) Attempt any Three questions out of the remaining Five questions.
(3) Figures to the right indicate full marks.
(4) Make suitable assumptions wherever necessary.

Q1 Answer the following sub-questions (Any Five) 20
(a) A steel tube having $\mathrm{k}=46 \mathrm{~W} / \mathrm{m}-{ }^{\circ} \mathrm{C}$ has an inside diameter of 3.0 cm and a tube wall thickness of 2 mm . A fluid flows on the inside of the tube producing a convection coefficient of $1500 \mathrm{~W} / \mathrm{m}^{2}$ Con the inside surface, while a second fluid flows across the outside of the tube producing a convection coefficient of $197 \mathrm{~W} / \mathrm{m}^{2}$. "C on the outside tube surface. The inside fluid temperature is $223^{\circ} \mathrm{C}$ while the outside fluid Temperature is $57^{\circ} \mathrm{C}$. Calculate the heat lost by the tube per meter of length.
(b) Give the physical significance of the following numbers-

1. Grashoff's Number
2. Prandtl Number
3. Nusselt's Number
4. Stanton Number
(c) Explain Kerns Method for design of heat exchanger.
(d) Differentiate between Film wise and Dropwise Condensation.
(e) Write a short note on Boiling Point Elevation of solution in Evaporator.
(f) Explain the Laws of Radiation

Q2
(a) Derive the expression for heat transfer through furnace wall made of three different materials in series. Assume K1, K2, K3, be the thermal conductivities of materials and $\mathrm{X} 1, \mathrm{X} 2, \mathrm{X} 3$, be the respective thickness. hi, and ho be the convective heat transfer coefficients for inside hot gas and ambient air respectively?
(b) A steel ball 50 mm in diameter and initially at uniform temp. of 723 K is suddenly placed in a controlled environment in which is maintained at 373 K . Calculate the time required for a ball to attain a temperature of 423 K .
Data- K for steel $=35 \mathrm{~W} / \mathrm{mK}, \quad$ Specific heat $=0.16 \mathrm{KJ} / \mathrm{KgK}$, $\mathrm{h}=10 \mathrm{~W} / \mathrm{m} 2 \mathrm{~K}$,

Density of steel $=7800 \mathrm{Kg} / \mathrm{m} 3$
(a) Derive an expression of LMTD for Counter Current Flow. Clearly state the assumption made.
(b) A circular disc insulated from the other side of the diameter is exposed to air at 293 K . If the disc diameter is maintained at 393 K , calculate the amount of heat transferred from it when,
[1] The Disc is horizontal with a hot surface facing upward.
[2] The Disc is horizontal with a hot surface facing downward.
[3] The Disc is vertical.
(a) A counter flow heat exchanger is used to heat water from $20^{\circ} \mathrm{C}$ to $80^{\circ} \mathrm{C}$ at a rate of $1.2 \mathrm{~kg} / \mathrm{s}$. The heating is obtained by using geothermal water available at $160^{\circ} \mathrm{C}$ at a mass flow rate of $2 \mathrm{~kg} / \mathrm{s}$. The inner tube is thin walled, and has a diameter of 1.5 cm . If the overall heat transfer coefficient is $640 \mathrm{~W} / \mathrm{m}^{2} \mathrm{~K}$. Calculate the length of the heat exchanger required to achieve the desired heating by using effectiveness-NTU method.
Take specific heat of geothermal water as $4.31 \mathrm{~kJ} / \mathrm{kg} \mathrm{K}$ and that of ground water as $4.18 \mathrm{~kJ} / \mathrm{kg}$ K
(b) Liquid oxygen at atmospheric pressure (boiling point $=90 \mathrm{~K}$ ) is stored in a spherical vessel of 300 mm outside diameter. The system is insulated by enclosing the container inside another concentric sphere of 500 mm inside diameter with the space between them evacuated. Both the sphere surfaces are made of aluminum for which emissivity may be taken as 0.3 . The temperature of the outer sphere is 313 K .
(i) Calculate the rate of heat flow by radiation.
(ii) What will be the reduction in the heat flow if polished aluminum with an emissivity of 0.5 is used for the container walls?
(a) A steam condenser consists of 16 tubes arranged in $4 \times 4$ array. The tubes are 25 mm in diameter and 1.2 m long. Water flows through the tube at $65^{\circ} \mathrm{C}$ while steam condenses at $75^{\circ} \mathrm{C}$ over the tube surface. Find the rate of condensation, if (a) tubes are horizontal; (b) tube are vertical.
Take latent heat of steam as $2300 \mathrm{~kJ} / \mathrm{kg}$ and properties of water at $70^{\circ} \mathrm{C}$ :
$\rho=977.8 \mathrm{~kg} / \mathrm{m}^{3}, \mathrm{Cp}=4.187 \mathrm{~kJ} / \mathrm{kg} \mathrm{K}, \mathrm{v}=0.415 \times 10-6 \mathrm{~m}^{2} / \mathrm{s}, \mathrm{k}=0.668 \mathrm{~W} / \mathrm{m} . \mathrm{K}$, $\beta=5.7 \times 10^{-3} \mathrm{~K}^{-1}$
(b) A heat exchanger contains 4500 tubes, each having a diameter of 2.54 cm , through which $11.3 \mathrm{~kg} / \mathrm{s}$ of air to be cooled from $538^{\circ} \mathrm{C}$ to $148^{\circ} \mathrm{C}$. Water passes in counter flow over the tubes, rising in temperature from $38^{\circ} \mathrm{C}$ to $85^{\circ} \mathrm{C}$. Determine the tube length required for this duty, if the water side resistance to heat flow is negligible. The physical properties of air at average temperature are as: $\rho=1.009 \mathrm{~kg} / \mathrm{m}^{3}, \mu=2.075 \times 10-5 \mathrm{~kg} / \mathrm{ms}, \mathrm{k}=3.003 \times 10-5$ $\mathrm{kW} / \mathrm{m} . \mathrm{K}, \mathrm{Cp}=1.0082 \mathrm{~kJ} / \mathrm{kg} . \mathrm{K}$.

For turbulent flow inside tubes, use relation
$\mathrm{Nu}=0.023 \operatorname{Re} 0.8 \operatorname{Pr} 0.4$
(a) A fine wire having a diameter of 0.02 mm is maintained at a constant temperature of $54^{\circ} \mathrm{C}$ by an electric current. The wire is exposed to air at 1 atm and $0^{\circ} \mathrm{C}$. Calculate the electric power necessary to maintain the wire temperature if the length is 50 cm .
Properties at average temperature:
$\beta=0.00333, \vartheta=15.69 \times 10^{-6} \mathrm{~m}^{2} / \mathrm{s}, \mathrm{K}=0.02624 \mathrm{~W} / \mathrm{m}^{\circ} \mathrm{C}, \operatorname{Pr}=0.708$.
(b) For Parallel flow heat exchanger Show that

$$
\varepsilon=\frac{e^{-N T U(1+C)}}{1+C}
$$

