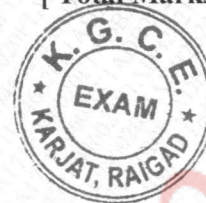


[3 Hours]

[ Total Marks: 80



- N. B :** (1) Question no.1 is **Compulsory**.  
(2) Attempt any **THREE** from question no.2 to 6.  
(3) Use illustrative diagrams wherever possible.  
(4) Assume suitable data if necessary and mention it clearly.  
(5) Use of steam table is permitted.

- Q.1 Answer any **Four** questions : 20
- What is the mode of heat transfer in vacuum? Define absorptivity, reflectivity and transmissivity and establish the relation among them.
  - Differentiate between the mechanism of filmwise and dropwise condensation.
  - What are the various types of fins? Discuss some of the important applications of fins
  - What is Heat exchanger? Draw Temperature profile for Parallel flow and Counter flow heat exchanger, Condenser, Evaporator.
  - A large window glass 0.5 cm thick ( $k = 0.78 \text{ W/m.K}$ ) of heat transfer area of  $1 \text{ m}^2$  is exposed to warm air at  $25^\circ\text{C}$ , over its inner surface, with convection coefficient of  $15 \text{ W/m}^2\text{.K}$ . The outer air is at  $-15^\circ\text{C}$  with convection coefficient of  $50 \text{ W/m}^2\text{.K}$ . Determine the heat flow rate through the glass.
- Q.2 a) A steam pipe of length 1m and 5cm inside diameter and 6.5 cm outside diameter is insulated with a 2.75 cm radial thickness of high temperature insulation ( $k= 1.1 \text{ W/m.K}$ ). The surface heat transfer coefficient for inside and outside surfaces are  $4650 \text{ W/m}^2\text{.K}$  and  $11.5 \text{ W/m}^2\text{.K}$ , respectively. The thermal conductivity of pipe material is  $45 \text{ W/m.K}$ . If the steam temperature is  $200^\circ\text{C}$  and ambient air temperature is  $25^\circ\text{C}$ , determine ;i) Heat lost per metre length of pipe ii) Temperature at the interface iii) Overall heat transfer coefficient based on inner and outer radius 12
- b) Write short note on- 8
- Lump system analysis
  - Heisler charts
- Q.3 a) Air at  $27^\circ\text{C}$  is flowing across a tube with a velocity of 25 m/s. The tube could be either a square of 5 cm side or a circular cylinder of 5 cm diameter. Compare the rate of heat transfer in each case, if the tube surface is at  $127^\circ\text{C}$ . 10
- Use  $Nu = C (Re)^n (Pr)^{1/3}$   
Where,  $C = 0.027$ ,  $n = 0.805$  for cylinder  
 $C = 0.102$ ,  $n = 0.675$  for square tube.  
Properties of air at  $77^\circ\text{C}$ ,  
 $\rho = 0.955 \text{ kg/m}^3$ ,  $k_f = 0.03 \text{ W/mK}$ ,  $\nu = 20.92 \times 10^{-6} \text{ m}^2/\text{s}$ ,  $Pr = 0.7$ ,  
 $C_p = 1.009 \text{ kJ/kgK}$ .
- b) Prove that the total emissive power (E) of a diffuse surface is equal to  $\pi$  times its intensity of radiation (I).

- Q.4 a) Steam in a condenser of a steam power plant is to be condensed at a temperature of  $30^{\circ}\text{C}$  with a cooling water from nearby lake, which enters the tube of condenser at  $14^{\circ}\text{C}$  and leaves at  $22^{\circ}\text{C}$ . The surface area of the tubes is  $45\text{ m}^2$  and an overall heat transfer coefficient is  $2100\text{ W/m}^2\text{K}$ . Calculate the mass flow rate of cooling water needed and rate of steam condensation in the condenser. Treat the condenser as counter flow heat exchanger.  $C_p$  of water at  $18^{\circ}\text{C}$  is  $4.18\text{ kJ/kg.K}$  and latent heat of vaporization at  $30^{\circ}\text{C}$  is  $h_{fg} = 2430.5\text{ kJ/kg}$  10
- b) State and explain the following laws- 6
- Planck's law
  - Stefan Boltzman law
- c) Explain time constant of a thermocouple. 4
- Q.5 a) An enclosure measures  $1.5\text{ m} \times 1.75\text{ m}$  with a height of  $2\text{ m}$ . Under steady state equilibrium conditions, the wall and ceiling are maintained at  $525\text{ K}$  and floor at  $400\text{ K}$ . Determine the net radiation to floor.  $\epsilon_1$  (emissivity of ceiling and wall)  $= 0.85$   $\epsilon_2$  (emissivity of floor)  $= 0.75$   $\sigma$  (Stefan-Boltzman constant)  $= 5.67 \times 10^{-8}\text{ W/m}^2\text{ K}^4$  6
- b) The inside temperature of furnace wall,  $200\text{ mm}$  thick, is  $1350^{\circ}\text{C}$ . The mean thermal conductivity of wall material is  $1.35\text{ W/m}^{\circ}\text{C}$ . The heat transfer coefficient of the outside surface is a function of temperature difference and is given by  $h = 7.85 + 0.08\Delta t$  where  $\Delta t$  is the temperature difference between outside wall surface and surroundings. Determine the rate of heat transfer per unit area if the surrounding temperature is  $40^{\circ}\text{C}$ . 6
- c) Derive an expression for the effectiveness of a parallel flow heat exchanger in terms of the number of transfer units (NTU) and the capacity ratio  $[C_{\min}/C_{\max}]$ . 8
- Q.6 a) Explain physical significance of i) Reynold's number ii) Nusselt's number 4
- b) In a quenching process a copper plate of  $3\text{ mm}$  thick is heated up to  $350^{\circ}\text{C}$  and then suddenly, it is dropped into a water bath at  $25^{\circ}\text{C}$ . Calculate the time required for the plate to reach the temperature of  $50^{\circ}\text{C}$ . The heat transfer coefficient on the surface of the plate is  $28\text{ W/m}^2\text{K}$ . The plate dimensions may be taken as length  $40\text{ cm}$  and width  $30\text{ cm}$ . Take the properties of copper as  $C = 380\text{ J/kg.K}$ ,  $\rho = 8800\text{ kg/m}^3$ ,  $k = 385\text{ W/m.K}$  8
- c) Explain shape factor and its properties. Find the shape factor of a cylindrical cavity (enclosed on its surface with a flat surface) of diameter  $d$  and depth  $h$  with respect to itself. 8